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Phase, Microstructure and Beneficiation of Manganese Ore by Acid Leaching

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Abstract

In this research work, sawdust was used as a reducing agent for sulphuric acid leaching of manganese ore from Prang Ghar, Lower Mohmand Agency, Pakistan. X-ray diffraction of the powdered sample indicated the presence of Hausmannite (Mn_3O_4), Calcium Aluminum Silicate Hydrate, Silica (SiO_2) and Hematite (Fe_2O_3). X-ray diffraction and the energy dispersive spectroscopic analysis show that the manganese ore sample was siliceous in nature. In the present study, six process parameters were investigated *i.e.* the particle size of the ore, leaching temperature, time duration, Mn ore amount, sulphuric acid concentration and amount of sawdust. Manganese extraction of 88.93 (wt%) was achieved for a leaching time of 60 minutes at 120 °C using 5% (v/v) H_2SO_4 concentration for 10 g Mn ore and 5 g sawdust. The results demonstrate that sawdust is a low cost, renewable and non-hazardous reducing agent in comparison to other available reagents.

Keywords

Siliceous Manganese Ore, Characterization, Leaching, Sawdust, Sulfuric Acid

1. Introduction

Manganese is an important element with a number of uses in major industrial applications *i.e.* production of steel, preparation of dietary additives, fertilizers, dry cells, paint production, animal feeds, textile dyes, medicines and colorants for bricks. Low-grade manganese ore can be treated either by reductive roasting or by reductive acid leaching [1] [2] [3]. Depletion of high grade Mn-ore has forced industry to use low and medium grade ore as raw material for the growing demands of steel and chemical industry. Since manganese dioxide ores are highly stable in acidic or alkaline oxidizing conditions, therefore its extraction should be carried out in reducing environment [2].

Using glucose as reducing agent in dilute nitric acid medium at 90° C for 32 h, 99% manganese has been extracted. It is concluded that high grade manganese can be obtained using nitric acid instead of sulphuric acid [4]. Kelong *et al.*, reported that using sawdust and rice husk as reductant in sulphuric acid medium, 95% manganese can be leached out. The influencing factors included pyrolusite and plant powder charge, sulphuric acid volume, temperature and duration of leaching [5]. Hariprasad *et al.*, reported that ~98% manganese can be extracted after leaching for 8 h using sawdust as reducing agent in sulphuric acid medium. Optimum leaching was reported for 5% H_2SO_4 (v/v) and 5% sawdust (w/w) at 90° C [6].

Using cane molasses as reducing agent in nitric acid medium raises manganese content from 37.5% to ~98% at optimum conditions of 2.7 M HNO₃, cane molasses 20% by weight, grain size 74 μ m, solid/liquid ratio 1:12 for 2 h at 95 °C [7]. Some biomass wastes such as sawdust, cane molasses, corncob, cornstalks, rice husk, wheat stalks, bagasse, bamboo, and shredded paper are environment-friendly and low-cost reducing agents for roasting reduction and leaching of manganese dioxide ore [8] [9].

In the present work, sawdust was used as a reducing agent in dilute sulfuric acid medium to extract manganese from ferromanganese ores. The use of sawdust for reduction of manganese dioxide is a simple, low cost and economical method in comparison to the other reductants.

2. Materials and Methods

Representative sample of manganese ore was collected from Prang Ghar $(34^{\circ}25'N, 71^{\circ}37'3''E)$, Upper Mohmand Agency, Khyber Pukhtunkhwa (KP), Pakistan. Manganese ore was crushed, grinded and then passed through 149 and 74 μ m sieves. Semi-quantitative EDS detected 24.05 wt% Mn, 21.15 wt% Ca, 15.24 wt% Si, 6.87 wt% Al, 29.44 wt% Fe and 3.25 wt% Mg in as-mined ore sieved at 74 μ m.

The leaching experiments were performed in a 500 mL glass beaker kept on a ceramic hot plate and magnetic stirring system in a fume hood. Initially 100 mL solution 5% (v/v) H₂SO₄ (5 mL H₂SO₄ and 95 mL distal water) was mixed thoroughly with weighed amount of sawdust (3, 4 and 5 g) to release glucose into the acid. After 15 min, the weighed amount of ore powder was transferred to the pulp. The leaching experiments were carried out for different sets of parameters *i.e.* particle size of Mn ore, leaching temperature, leaching time, Mn ore amount, sulphuric acid concentration and amount of sawdust.

Room temperature X-rays diffraction (XRD) data were recorded using a JEOL JDX-3532 X-ray diffractometer, operating at 40 kV and 30 mA, with Cu K α radiation (λ ~0.154 nm) at Centralized Resource Laboratory (CRL), University of Peshawar, Pakistan. The samples were scanned from 10° - 70° (2 θ) with a count time/step of 1.25 s and 0.02° step size. Secondary electron scanning electron microscope (SEM) images of chemically etched samples were recorded using a

JEOL JSM5910 SEM, operating at 30 keV. Semi-quantitative energy dispersive X-ray electron spectroscopy (EDS) data were collected using an INCA200 EDS detector (Oxford instruments, UK), connected with a JEOL-JSM5910 SEM. A PMG-3 microscope coupled with a DP-12 CCD camera, Olympus (Japan) was used for recording optical images in the present study at CRL.

3. Results and Discussion

3.1. Characterization of As-Mined Samples

Figure 1 shows the reflected light micrograph of as-mined manganese ore sample. Three types of micro-regions were observed to have different contrast, microstructure and texture.

The long and straight dark thick strip marked as "A" crossing two different types of regions (appearing light greenish dark region with granular morphology and the plane white region) may be due to the combination of oxides of manganese and iron that impart iron black color [2]. The white to bluish grey colored micro-regions marked as B and C may be the maghemite (iron rich) phase as it gives rise to a similar color/contrast under reflected light [3]. The boundaries of the micro-regions B and C were sharp and could be distinguished from one another.

Figure 2 shows a secondary electron SEM image (SEI) of as-mined ore sample showing three distinct micro-regions. Light grey irregular shape manganese rich micro-regions with spongy texture marked as A and C. The light grey cuboidal

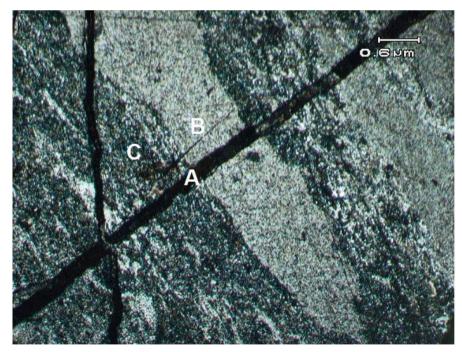


Figure 1. Reflected light micrograph of as-mined manganese ore sample showing microregions with different morphology and appearance. Long and jet dark strips marked as "A" is Mn rich while white to bluish grey micro-regions marked as "B" and "C" may be due to iron rich maghemite.

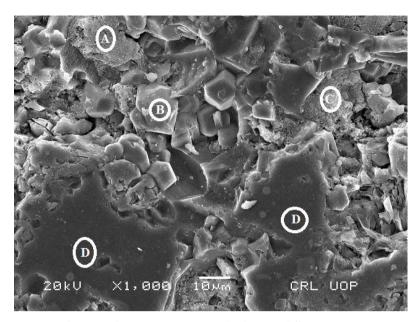


Figure 2. SEI of as-mined manganese ore sample showing different micro-regions, manganese rich micro-region marked as A & C, pure silica region with blackish appearance marked as D and cuboidal grain marked as B.

Table 1. Elemental composition of different micro-regions shown in Figure 2.

El (D)	Elemental concentration (wt%)					
Elements/Region	Mg	Al	Si	Ca	Fe	Mn
Gross composition	3.25	6.87	15.24	21.15	29.44	24.05
A			10.16	9.14	20.30	60.40
В		16.07	31.61	4.86	8.51	38.95
С		17.35	30.51	7.47		44.67
D			100			

or pseudo-hexagonal grains labeled as B and dark grey silica rich plane microregion labeled as D. The elemental compositions of these micro-regions are given in **Table 1**.

Figure 3 shows room temprature XRD pattern recorded for as-mined manganese ore. The inter-planner spacing (d-values) and relative intensities corresponding to the major XRD peaks (labled as **a**) recorded for manganese ore matched PDF # 75-1560 for Mn₃O₄ indicating it to be the major phase in the examined sample. Additionally, some minor peaks (labeled as **b, c** and **d**) matched PDF # 20-452 for Calcium Aluminum Silicate Hydrate, PDF# 38-360 for SiO₂ and PDF # 6-502 for Hematite (Fe₂O₃) showing these to be minor phases of gangue minerals. **Table 2** shows a comparison of mineralogical and elemental analysis by XRD and EDS respectively.

Using XRD Cheng *et al.* reported the presence of pyrolusite (MnO_2) as the major phase along with small amounts of MgO, silica (SiO_2) , hematite (Fe_2O_3) and Al_2O_3 in manganese ore from Guangxi, China [10]. Another XRD study of

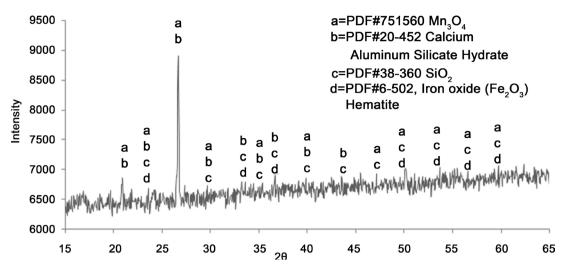


Figure 3. XRD patterns of as-mined manganese ore showing different phases marked as a, b, c & d.

Table 2. Elementa	l and minera	logical analy	ysis by EDS	and XRD.

EDS ana	llysis	XRD analysis		
Elements	Wt%	Mineral	Formula	PDF#
Si	15.24	Quartz	SiO ₂	38 - 360
Mn	24.05	Hausmanite	$\mathrm{Mn_3O_4}$	75 - 1560
Fe	29.44	Hematite	Fe_2O_3	6 - 502
Al	2.87	Calcium aluminium silicate hydrate 20-		20, 452
Ca	22.40			20-452

low-grade manganese ore from Guangxi, China reported the presence of todorokite ($Mn_6O_{12}\cdot4\cdot16H_2O$) and hematite (Fe_2O_3) as the major phases and the gangue minerals were quartz (SiO_2) and kaolinite ($Al_2Si_2O_5(OH)_4$) [11].

3.2. Characterization of Leached Manages Ore Samples

Basic chemical reaction for leaching of MnO_2 using sawdust $C_6H_{10}O_5$ can be as following

$$12\text{MnO}_2 + \text{C}_6\text{H}_{10}\text{O}_5 + 12\text{H}_2\text{SO}_4 \rightarrow 12\text{MnSO}_4 + 17\text{H}_2\text{O} + 6\text{CO}_2 \uparrow$$

 $C_6H_{10}O_5$ show that cellulose of sawdust contain α -D-glucose units. Acid treatment release glucose that acts as reducing agent [12].

3.3. Effect of Mesh Size

Influence of particle size of ore on efficiency of leaching was studied at 100, 200 and 300 mesh sizes while keeping the other parameters constant *i.e.* 5 g sawdust, 10 g Mn ore, 5% (v/v) H_2SO_4 , 90°C and 60 minutes leaching time.

Figure 4 shows an increase in Mn content and decrease of silica and iron when the particle size (particle diameter) of the ore was decreased. EDS results revealed beneficiation of Mn from 24.05 wt% to 73.28 wt% at particle size of 300 mesh. **Table 3** shows variation in elemental composition of Mn, Si and Fe at 100,

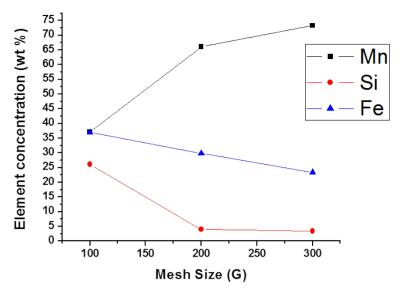


Figure 4. Variation of element concentration with mesh size.

Table 3. Elemental concentration at 100, 200 and 300 mesh size of leached Mn ore.

Mesh size	Ele	emental composition (w	t%)
Mesii size	Mn	Si	Fe
100	37.05	26.03	36.92
200	66.11	4.02	29.87
300	73.28	3.36	23.36

200 and 300 mesh sizes of manganese ore. An increase in leaching efficiency with increasing mesh size has been reported by Hariparsad *et al.*, and Tian *et al* [6] [8].

3.4. Effect of Sawdust Amount

Sulfuric acid cannot be used directly for leaching of manganese ores. However; reducing substances like sawdust can be used in acidic solution for high efficiency of manganese leaching.

For investigating the effect of sawdust, various leaching experiments were performed by changing sawdust concentration from 3.0 to 5.0 g/L while keeping other parameters fix *i.e.* 5 % (v/v) sulfuric acid concentration, leaching time of 60 min, manganese ore amount of 10 g, leaching temperature of 90°C and mesh size of 200.

Since XRD analysis confirmed the presence of hematite phase in manganese ore sample. However; crystalline nature of hematite requires a highly acidic medium due to its consumption of H^+ ions. Increasing the amount of sawdust at a certain temperature and acid concentration causes an increase in the leaching efficiency of Mn due to excess availability of H^+ ion concentration [13].

Table 4 gives variation in elemental composition of Mn, Si and Fe for 3, 4 and 5 g sawdust. **Figure 5** shows an increase in Mn content accompanied by decrease

Table 4. Elemental concentration of leached Mn-ore for 3 g, 4 g and 5 g of sawdust.

Sawdust amount	Elen	nental composition (v	wt%)
Sawdust amount	Mn	Si	Fe
3 g	32.82	10.61	56.57
4 g	37.02	36.29	26.68
5 g	66.11	4.02	29.87

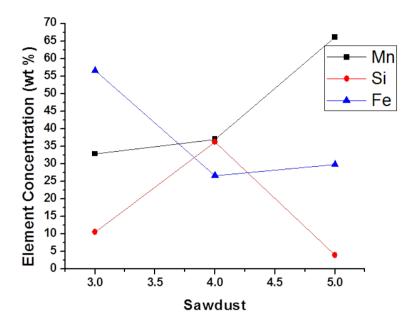


Figure 5. Efficiency of manganese ore leaching at varying amount of sawdust.

in both the Si and Fe concentrations by increasing the sawdust amount.

3.5. Effect of Temperature on Manganese Ore Leaching

The influence of leaching temperature on leaching efficiency at 60° C, 90° C and 120° C was investigated while keeping the other parameters constant *i.e.* 5 g sawdust, 5 % (v/v) concentration of H₂SO₄, leaching time of 60 min, 10 g Mn-ore of 200 mesh size.

Table 5 shows the observed variation in the elemental composition of Mn, Si and Fe for manganese ore treated at 60°C, 90°C and 120°C. **Figure 6** shows variation in the elemental composition with temperature. The graph indicated that manganese concentration was lower at low temperature and increased with an increase in the leaching temperature; similarly the concentration of silicon and iron decreased with increasing temperature.

3.6. Influence of Time on Leaching of Manganese Ore

Three sets of experiments were performed in order to study the influence of time on leaching efficiency of manganese ore. The ore sample was treated for 1 h, 2 h and 3 h at constant sawdust amount 5 g, sulfuric acid concentration 5 % (v/v), leaching temperature 90° C and 200 mesh size Mn-ore = 10 g.

Table 5. Elemental concentration of leached Mn-ore sample at 60°C, 90°C and 120°C temperature.

TT	Ele	Elemental composition (wt%)		
Temperature	Mn	Si	Fe	
60°C	43.17	27.63	19.20	
90°C	66.11	4.02	29.87	
120°C	88.93	2.12	8.95	

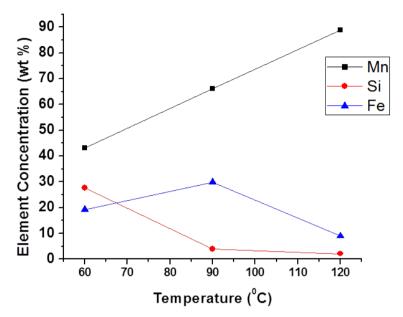


Figure 6. Effect of temperature on elemental concentration of the samples.

Table 6. The elemental concentration of Mn ore sample leached at 1 h, 2 h and 3 h.

Time -		Elemental composition	
i iiie	Mn	Si	Fe
1 h	66.11	4.02	29.87
2 h	74.11	8.24	17.65
3 h	83.35	6.61	10.04

Table 6 gives the quantitative variation in the elemental concentration of Mn, Si and Fe. Figure 7 shows the graph for variation in elemental concentration of the leached samples with change in leaching time. It was observed that by increasing time duration from 1 - 3 h the recovery increased from 66 to 83 wt%, consistent with the previous study.

3.7. Effect of Manganese Ore Amount

Leaching experiments were also performed for 10 g, 15 g and 20 g 200 mesh Mn ore samples at fixed values of 5% (v/v) $\rm H_2SO_4$, 5 g sawdust, 90°C temperature and 1 h leaching time.

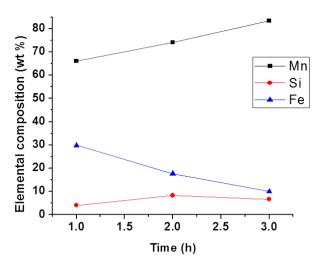


Figure 7. Effect of leaching time on the elemental concentration of Mn-ore.

Table 7. The elemental concentration of 10 g, 15 g and 20 g Mn ore sample.

Ore amount	Elemental composition			
Ore amount	Mn	Si	Fe	
10 g	66.11	4.02	29.87	
15 g	68.71	14.49	16.79	
20 g	62.44	11.78	25.78	

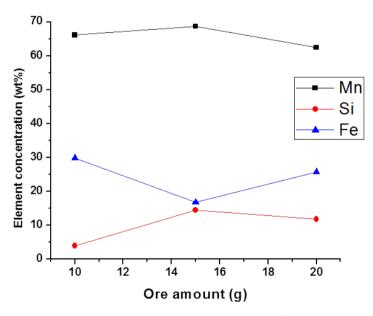


Figure 8. Effect of ore amount on the elemental concentration of leached Mn-ore samples.

Table 7 gives the elemental and oxide compositions of Mn, Si and Fe for 10, 15 and 20 g of Mn ore.

Figure 8 shows the observed variation in the elemental concentration of Mn, Si and Fe. These experiments demonstrated that by increasing the manganese ore amount the concentration of manganese decreased which may be due to in-

sufficient amount of acid or the reducing sugar generated from the smaller amount of sawdust in comparison to the ore amount.

3.8. Effect of H₂SO₄ Concentration

The influence of the amount of acid used on the leaching efficiency was also investigated. 5 mL, 10 mL and 15 mL $\rm H_2SO_4$ was used for 5 g sawdust, at 90°C leaching temperature, with a leaching time of 60 min and 200 mesh size 10 g Mn ore sample.

Table 8 gives elemental concentration and oxide compositions of Mn, Si and Fe measured by EDS for manganese ore treated with 5 mL, 10 mL and 15 mL H₂SO₄. Figure 9 shows the observed variation in elemental composition with acid concentration. EDS analysis showed that the leaching efficiency increased with an increase in the amount of acid used because the sawdust released glucose more rapidly than at relatively less acid.

4. Conclusions

In this study, manganese ore from Prang Ghar, Lower Mohmand agency, Pakistan was characterized using XRD, SEM, EDX and optical microscopy. Prang Ghar manganese ore is a low grade ferruginous manganese ore. The major non-

Table 8. Elemental concentration of Mn ore leached with 5 mL, 10 mL and 15 mL H₂SO₄.

H ₂ SO ₄ concentration	Elemental composition (wt%)			
	Mn	Si	Fe	
5 mL	66.11	4.02	29.87	
10 mL	76.21	16.19	7.61	
15 mL	80.77	8.63	10.60	

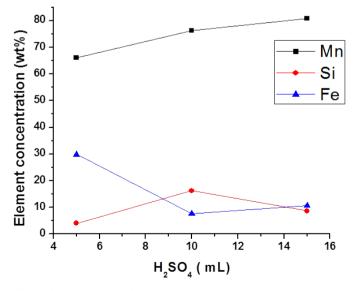


Figure 9. Effect of the amount of acid on the elemental concentration in the leached samples.

oxide elements detected by EDS in this ore are Manganese, Silicon and Iron. The mineralogy of manganese ore is complex. The constituent phases of manganese ore samples identified using XRD analysis are Hausmannite (Mn_3O_4), Calcium Aluminum Silicate Hydrate, Silica (SiO_2) and Hematite.

The chemical beneficiation of manganese ore was carried out using a commercial grade concentrated H₂SO₄ and sawdust as reductant. The investigated parameters included temperature; Mn ore mesh size and amount, leaching time, acid concentration and sawdust amount. The highest manganese concentration of 88.93 (wt%) was achieved at 120°C, 200 mesh size Mn ore, 60 minutes leaching time, 5% (v/v) H₂SO₄ and 5 g sawdust. Mn extraction increases with an increase in temperature, ore particle size, sawdust amount, time duration and the amount of acid. The observed decrease in Mn concentration with increasing Mn ore amount may be due to insufficient amount of acid or the reducing sugar generated from the sawdust. In all the experiments, the decrease in Si and Fe has been observed with increase in all the six parameters. Considering the observed productivity of the utilized sawdust, the process is beneficial from both the economic and environmental perspective.

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References

- [1] Sahoo, R.N., Naik, P.K. and Das, S.C. (2001) Leaching of Manganese Ore Using Oxalic Acid as Reductant in Sulphuric Acid Solution. *Hydrometallurgy*, **62**, 157-163. https://doi.org/10.1016/S0304-386X(01)00196-7
- [2] Sahoo, P.K. and Rao, K.S. (1989) Sulphating-Roasting of Low Grade Manganese Ore Optimisation by Factorial Design. *International Journal of Mineral Processing*, 25, 147-152. https://doi.org/10.1016/0301-7516(89)90061-6
- [3] Abbruzzese, C. (1987) Aqueous SO₂ Processing of Manganese Ores Separation Processes in Hydrometallurgy. Ellis Horwood Ltd., 77-87.
- [4] Pagnanelli, F., Furlani, G., Valentini, P., Veglio, F. and Toro, L. (2004) Leaching of Low-Grade Manganese Ores by Using Nitric Acid and Glucose Optimization of the Operating Conditions. 157-167.
- [5] Kelong, Y.Y.H. (2001) Test of Pyrolusite Direct Leaching in Sulphuric Acid with Addition of Plants Powder as Reducing Agents.
- [6] Hariparsad, D., Dash, B., Ghosh, M.K. and Anand, S. (2007) Leaching of Manganese Ore Using Sawdust as a Reductant. 1293-1295.
- [7] Lasheen, T.A., El-Hazek, M.N., Helal, A.S. and El-Nagar, W. (2009) Recovery of

- Manganese Using Molasses as Reductant in Nitric Acid Solution. *International Journal of Mineral Processing*, **92**, 109-114. https://doi.org/10.1016/j.minpro.2009.03.001
- [8] Tian, X., Wen, X., Yang, C., Liang, Y., Pi, Z. and Wang, Y. (2010) Reductive Leaching of Manganese from Low-Grade Manganese Dioxide Ores Using Corncob as Reductant in Sulfuric Acid Solution. *Hydrometallurgy*, 100, 157-160. https://doi.org/10.1016/j.hydromet.2009.11.008
- [9] Zhang, H., Zhu, G., Yan, H., Zhao, Y., Li, T. and Feng, X. (2013) Reduction of Low-Grade Manganese Dioxide Ore Pellets by Biomass Wheat Stalk. *Acta Metallur-gica Sinica*, 26, 167-172. https://doi.org/10.1007/s40195-012-0250-x
- [10] Cheng, Z., Zhu, G. and Zhao, Y. (2009) Study in Reduction-Roast Leaching Manganese from Low-Grade Manganese Dioxide Ores Using Cornstalk as Reductant. *Hydrometallurgy*, **96**, 176-179. https://doi.org/10.1016/j.hydromet.2008.08.004
- [11] Su, H., Wen, Y., Wang, F., Sun, Y. and Tong, Z. (2008) Reductive Leaching of Manganese from Low-Grade Manganese ore in H₂SO₄ Using Cane Molasses as Reductant. *Hydrometallurgy*, 93, 136-139. https://doi.org/10.1016/j.hydromet.2008.01.001
- [12] Van der, W., Mahabir, R.D., Abbadi, J. and Reuter, M.A. (2002) Copper Recovery from Cu Sulphate Solutions by Reduction with Carbohydrates. *Hydrometallurgy*, **64**, 131-146.
- [13] Momade, F.W.Y. and Momade, Zs.G. (1999) Reductive Leaching of Manganese Ore Inaqueous Methanol-Sulphuric Acid Medium. *Hydrometallurgy*, 51, 103-113. https://doi.org/10.1016/S0304-386X(98)00077-2